

Thermal Analysis and Modeling

- Cooling humans
- Fundamentals of heat transfer
- Radiative equilibrium
- Surface properties
- Non-ideal effects
- Conduction
- Human thermal modeling
- Thermal system components

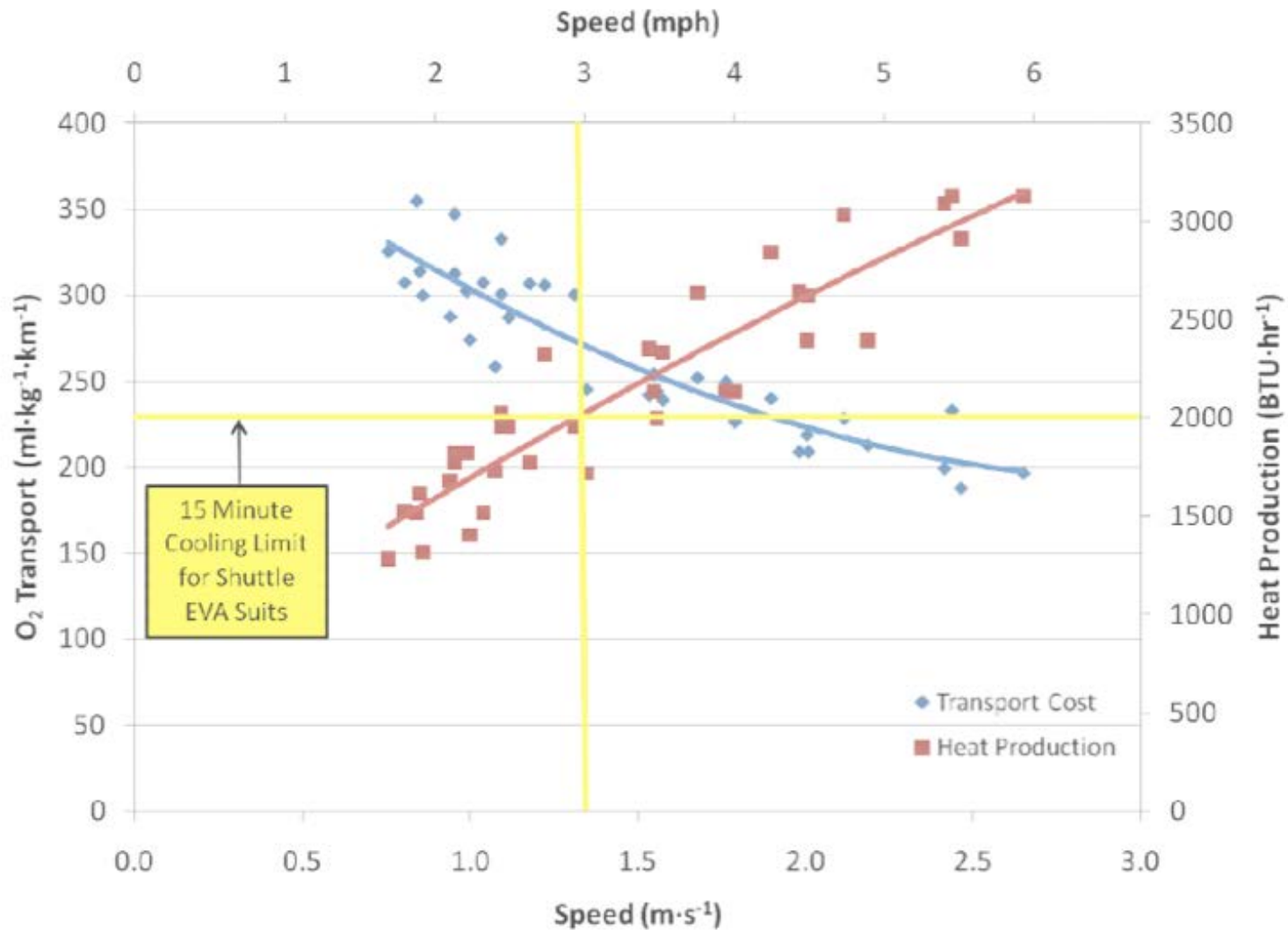
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UNIVERSITY OF
MARYLAND

Thermal Analysis and Modeling
ENAE 697 - Space Human Factors and Life Support

Cooling and Energy Use in Lunar Run



So What Is 2000 BTU?

- $2000 \text{ BTU/hr} = 504 \text{ kcal/hr}$ (or “calories” of food)
- Would heat 8 kg of water from body temperature (37°C) to boiling
- Water heat of vaporization = $2257 \text{ kJ/kg} = 535 \text{ kcal/kg}$
- Need to convert 0.94 kg of water to vapor
- At 70°F , air can hold 1.15 lbs of water per KCFM
- Suit flow rate of 6 CFM = 3 gms/minute = $0.19 \text{ kg/hr} = 100 \text{ kcal/hr} = 397 \text{ BTU/hr}$



Sublimation to Dump Heat

- Flow water over porous plate exposed on other side to vacuum
 - Water passing through pores evaporates in vacuum - cools at rate of 535 kcal/kg
 - Plate reaches 0°C and water in pores freezes
 - Water at vacuum surface sublimates (solid—>gas)
 - Heat of melting 80 kcal/kg
 - Heat of vaporization 535 kcal/kg
 - Total heat of sublimation 615 kcal/kg
- Cooling 2000 BTU/hr (504 kcal/hr) requires 0.82 kg of water (ideal case)



Apollo PLSS Sublimator



Sublimator Schematic

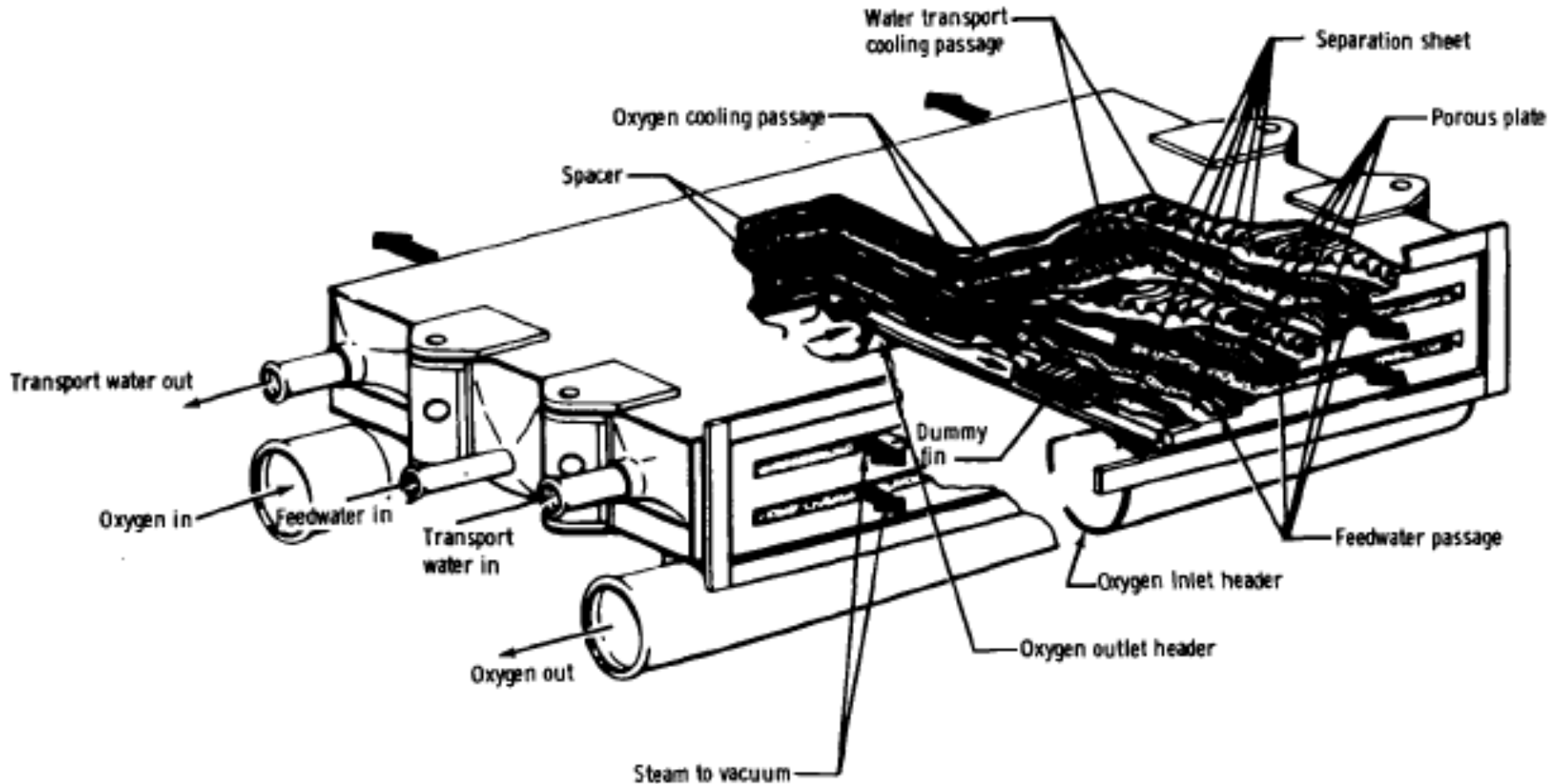


Figure 45. - Sectional view of the sublimator.



Sublimator Vapor “Cloud” on Moon



Past PLSS Thermal Capacities

- Apollo
 - 8 hrs @ 930 BTU/hr
 - 6 hrs @ 1200 BTU/hr
 - 5 hrs @ 1600 BTU/hr
- Shuttle/ISS EMU
 - 7 hrs @ 1000 BTU/hr (PLSS contains 3.9 kg of water - previous calculation predicts 2.87 kg)
- Advanced EMU (development)
 - 8 hrs @ 1200 BTU/hr

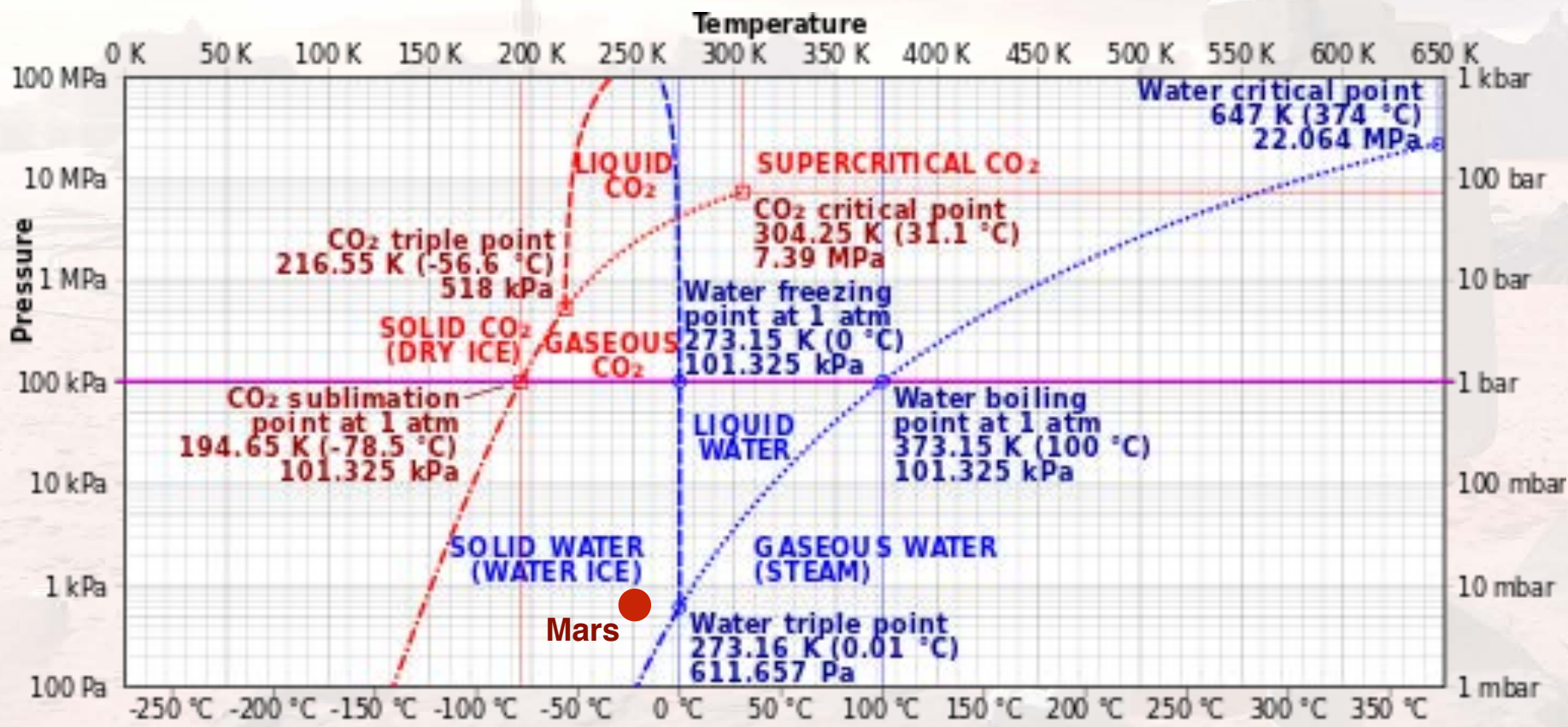


Issues with Sublimators

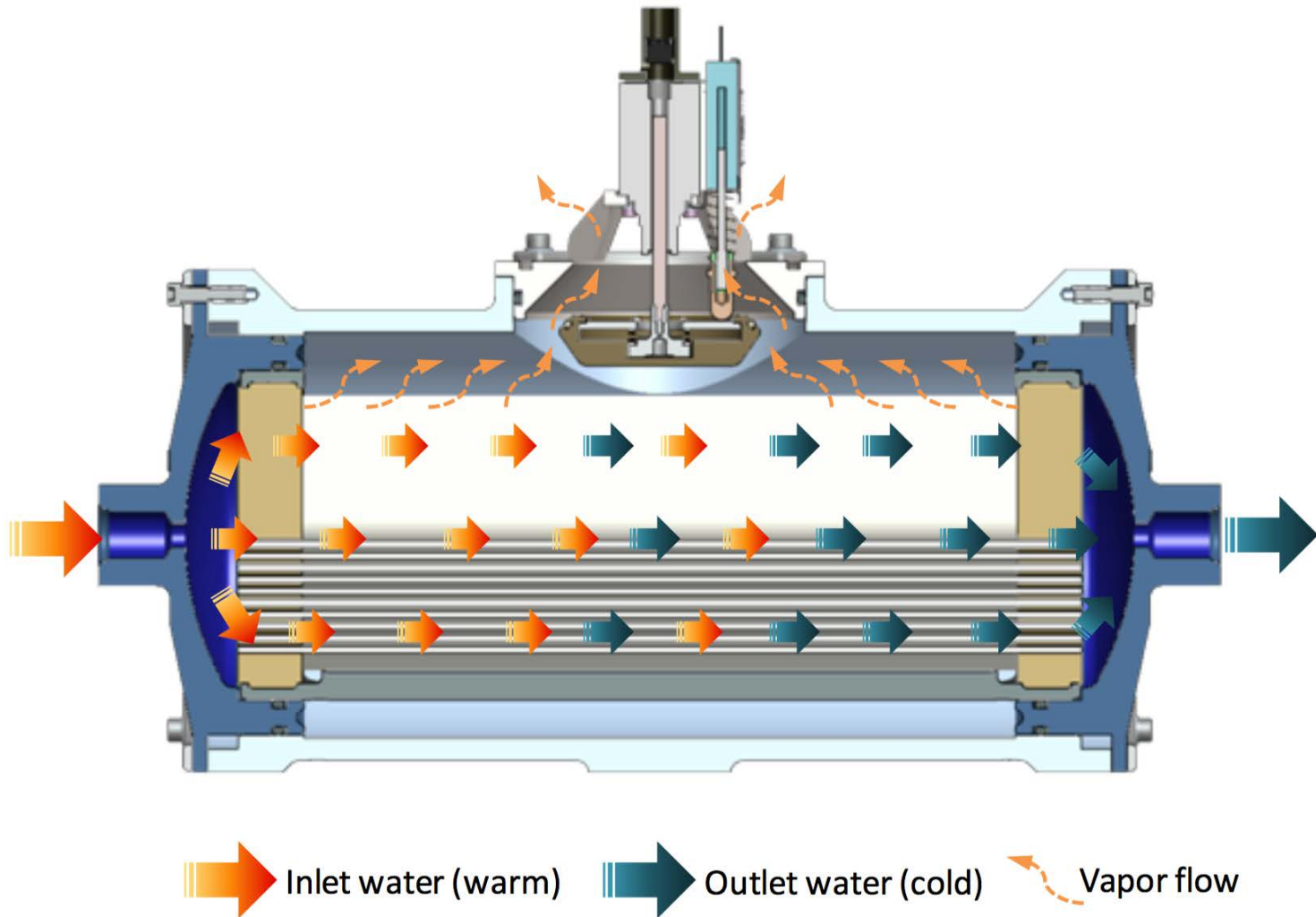
- Have to be “charged” - i.e., run water through long enough to freeze porous plate
- Susceptible to contamination damage (e.g., plugging pores in plate)
- Issues with liquid / gas separation (cooling both LCVG water and suit atmosphere)
- Only works in conditions below triple point of water



Phase Curves for CO₂ and H₂O



Suit Membrane Water Evaporator



Ref: Bue et.al., "Long-Duration Testing of a Spacesuit Water Membrane Evaporator Prototype" 42nd ICES, AIAA 2012-3459



SWME Fundamentals

- 14,900 hollow fibers carrying water for cooling
- Hydrophobic fiber material rejects water, but allows water vapor to pass
- Chamber pressure is controlled with a back-pressure regulator
- Rate of evaporation (and rate of cooling) controlled by internal pressure in chamber
- Evaporated vapor purged through regulator to ambient
- Evaporation provides 87% of sublimation cooling



Classical Methods of Heat Transfer

- Convection
 - Heat transferred to cooler surrounding gas, which creates currents to remove hot gas and supply new cool gas
 - Don't (in general) have surrounding gas or gravity for convective currents
- Conduction
 - Direct heat transfer between touching components
 - Primary heat flow mechanism internal to vehicle
- Radiation
 - Heat transferred by infrared radiation
 - Only mechanism for dumping heat external to vehicle



Ideal Radiative Heat Transfer

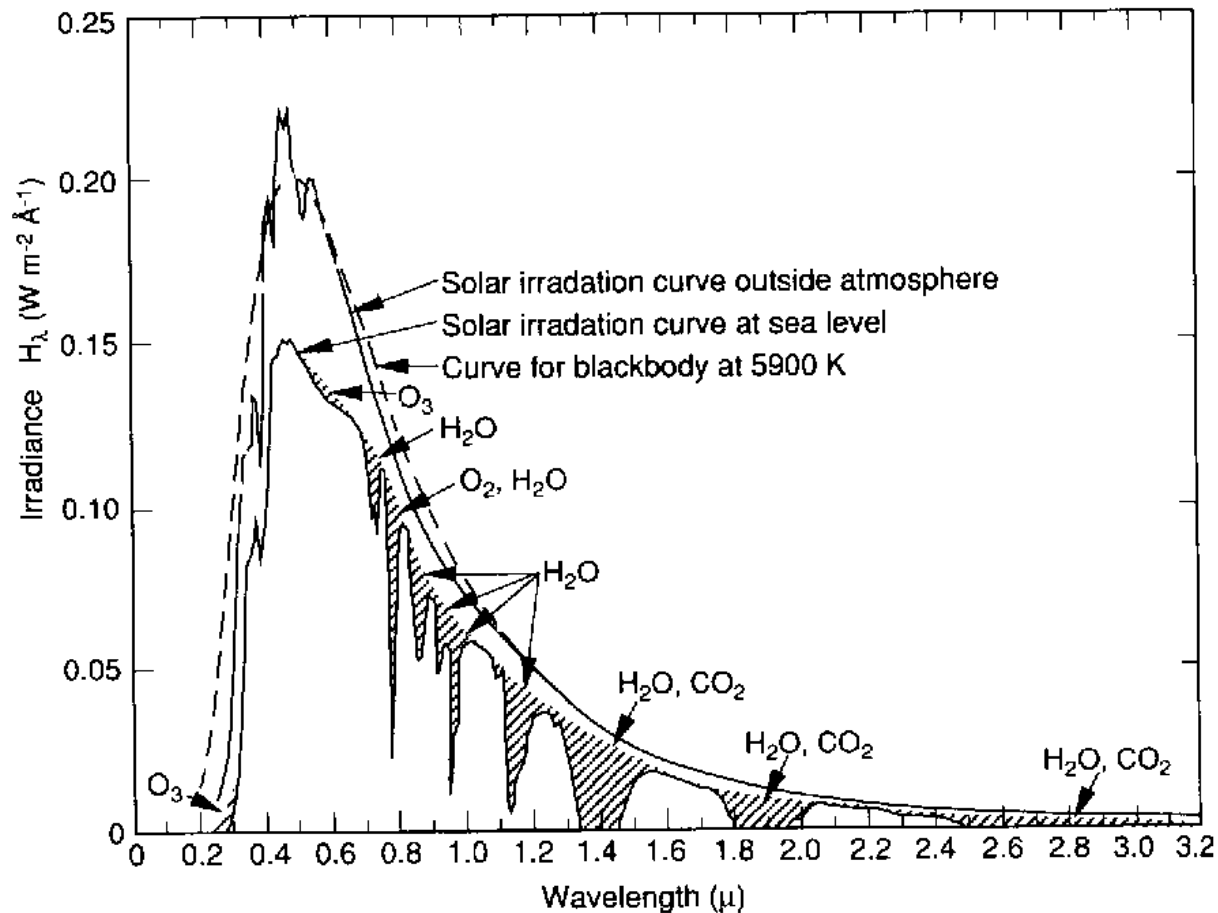
Planck's equation gives energy emitted in a specific frequency by a black body as a function of temperature

$$e_{\lambda b} = \frac{2\pi h C_0^2}{\lambda^5 \left[\exp\left(\frac{-h C_0}{\lambda k T}\right) - 1 \right]}$$

(Don't worry, we won't actually use this equation for anything...)



The Solar Spectrum



Ref: V. L. Pisacane and R. C. Moore, Fundamentals of Space Systems Oxford University Press, 1994



Ideal Radiative Heat Transfer

Planck's equation gives energy emitted in a specific frequency by a black body as a function of temperature

$$e_{\lambda b} = \frac{2\pi h C_0^2}{\lambda^5 \left[\exp\left(\frac{-h C_0}{\lambda k T}\right) - 1 \right]}$$

- Stefan-Boltzmann equation integrates Planck's equation over entire spectrum

$$P_{rad} = \sigma T^4$$

$$\sigma = 5.67 \times 10^{-8} \frac{W}{m^2 \circ K^4}$$

(“Stefan-Boltzmann Constant”)



Thermodynamic Equilibrium

- First Law of Thermodynamics

$$Q - W = \frac{dU}{dt}$$

heat in - heat out = work done internally

- Heat in = incident energy absorbed
- Heat out = radiated energy
- Work done internally = internal power used
(negative work in this sense - adds to total heat in the system)



Radiative Equilibrium Temperature

- Assume a spherical black body of radius r
- Heat in due to intercepted solar flux

$$Q_{in} = I_s \pi r^2$$

- Heat out due to radiation (from total surface area)

$$Q_{out} = 4\pi r^2 \sigma T^4$$

- For equilibrium, set equal

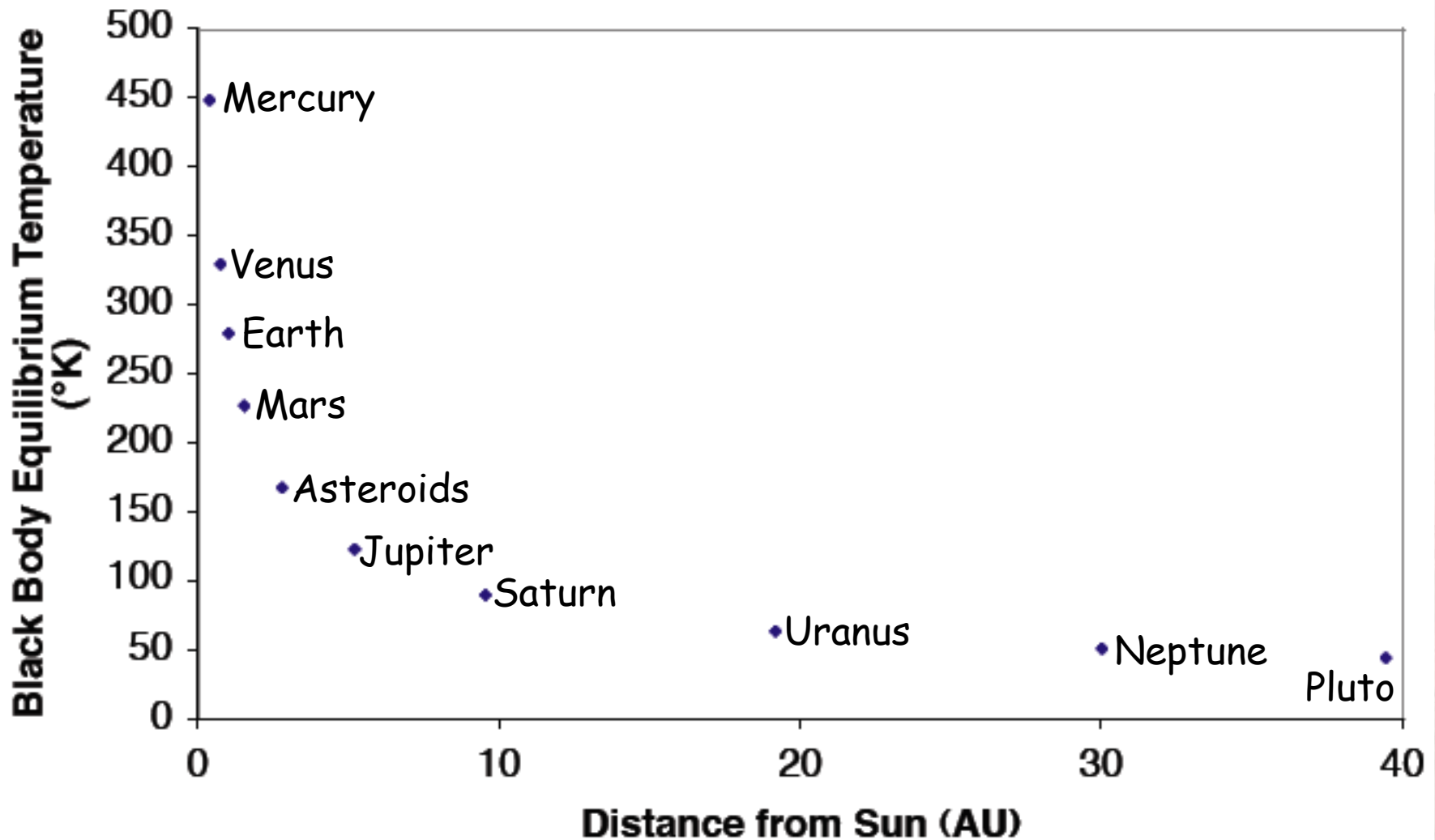
$$I_s \pi r^2 = 4\pi r^2 \sigma T^4 \Rightarrow I_s = 4\sigma T^4$$

- 1 AU: $I_s = 1394 \text{ W/m}^2$; $T_{eq} = 280^\circ\text{K}$

$$T_{eq} = \left(\frac{I_s}{4\sigma} \right)^{1/4}$$



Effect of Distance on Equilibrium

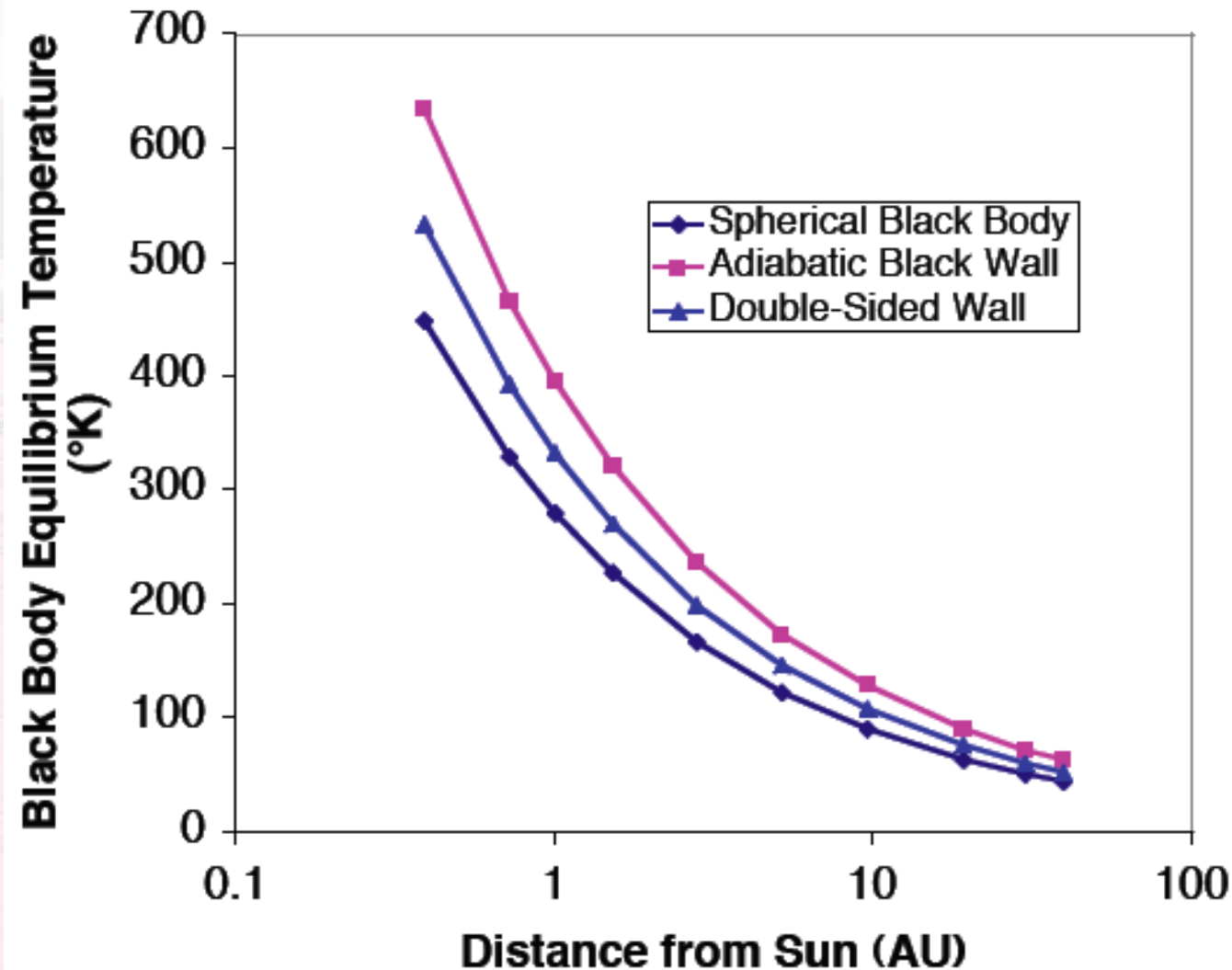


Shape and Radiative Equilibrium

- A shape absorbs energy only via illuminated faces
- A shape radiates energy via all surface area
- Basic assumption made is that black bodies are intrinsically isothermal (perfect and instantaneous conduction of heat internally to all faces)



Effect of Shape on Black Body Temps



Incident Radiation on Non-Ideal Bodies

Kirchhoff's Law for total incident energy flux on solid bodies:

$$Q_{Incident} = Q_{absorbed} + Q_{reflected} + Q_{transmitted}$$

$$\frac{Q_{absorbed}}{Q_{Incident}} + \frac{Q_{reflected}}{Q_{Incident}} + \frac{Q_{transmitted}}{Q_{Incident}} = 1$$

$$\alpha \equiv \frac{Q_{absorbed}}{Q_{Incident}}; \quad \rho \equiv \frac{Q_{reflected}}{Q_{Incident}}; \quad \tau \equiv \frac{Q_{transmitted}}{Q_{Incident}}$$

where

- α = absorptance (or absorptivity)
- ρ = reflectance (or reflectivity)
- τ = transmittance (or transmissivity)



Non-Ideal Radiative Equilibrium Temp

- Assume a spherical black body of radius r
- Heat in due to intercepted solar flux

$$Q_{in} = I_s \alpha \pi r^2$$

- Heat out due to radiation (from total surface area)

$$Q_{out} = 4\pi r^2 \varepsilon \sigma T^4$$

(ε = “emissivity” - efficiency of surface at radiating heat)

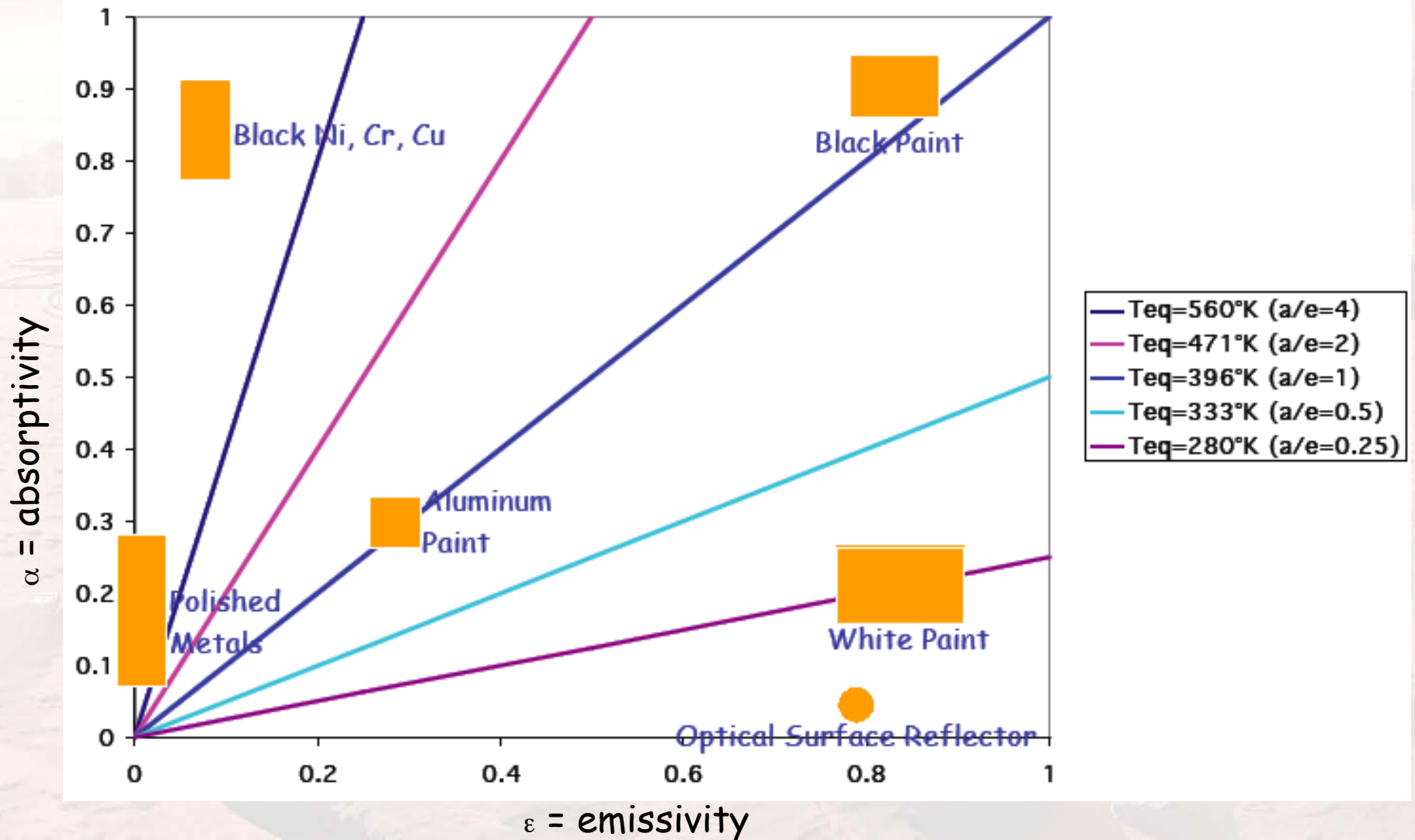
- For equilibrium, set equal

$$I_s \alpha \pi r^2 = 4\pi r^2 \varepsilon \sigma T^4 \Rightarrow I_s = 4 \frac{\varepsilon}{\alpha} \sigma T^4$$

$$T_{eq} = \left(\frac{\alpha}{\varepsilon} \frac{I_s}{4\sigma} \right)^{1/4}$$



Effect of Surface Coating on Temperature



Non-Ideal Radiative Heat Transfer

- Full form of the Stefan-Boltzmann equation

$$P_{rad} = \epsilon \sigma A (T^4 - T_{env}^4)$$

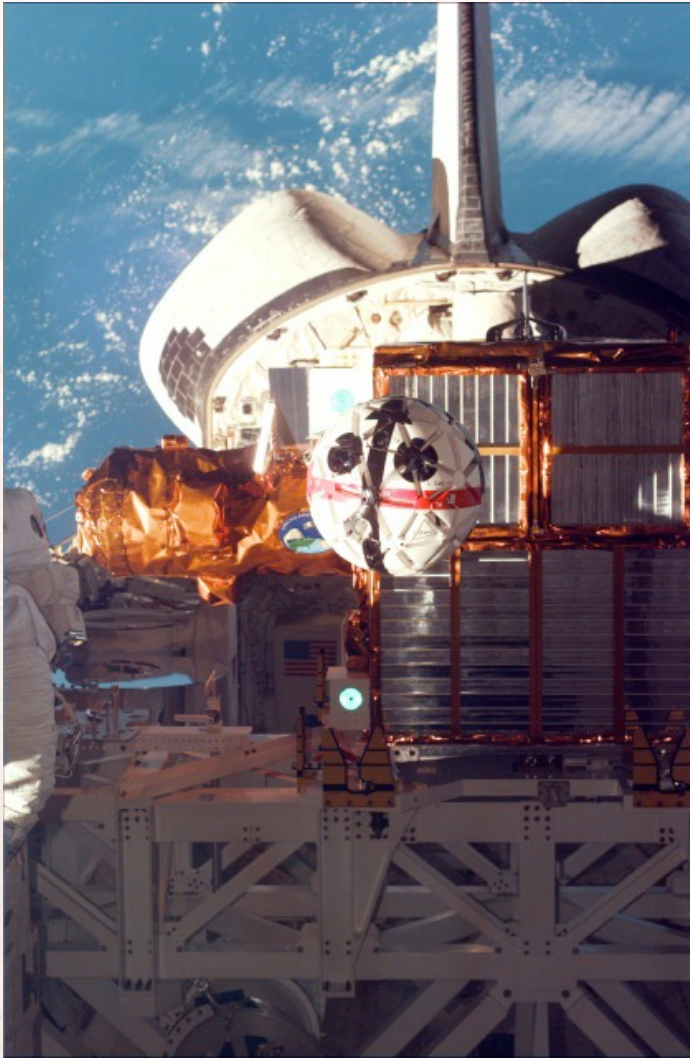
where T_{env} = environmental temperature (=4°K for space)

- Also take into account power used internally

$$I_s \alpha A_s + P_{int} = \epsilon \sigma A_{rad} (T^4 - T_{env}^4)$$



Example: AERCam/SPRINT



- 30 cm diameter sphere
- $\alpha=0.2$; $\varepsilon=0.8$
- $P_{\text{int}}=200\text{W}$
- $T_{\text{env}}=280^{\circ}\text{K}$ (cargo bay below; Earth above)
- Analysis cases:
 - Free space w/o sun
 - Free space w/sun
 - Earth orbit w/o sun
 - Earth orbit w/sun



AERCam/SPRINT Analysis (Free Space)

- $A_s=0.0707 \text{ m}^2$; $A_{\text{rad}}=0.2827 \text{ m}^2$
- Free space, no sun

$$P_{\text{int}} = \epsilon \sigma A_{\text{rad}} T^4 \Rightarrow T = \left(\frac{200 \text{ W}}{0.8 \left(5.67 \times 10^{-8} \frac{\text{W}}{\text{m}^2 \cdot \text{K}^4} \right) (0.2827 \text{ m}^2)} \right)^{1/4} = 354^\circ \text{K}$$



AERCam/SPRINT Analysis (Free Space)

- $A_s=0.0707 \text{ m}^2$; $A_{\text{rad}}=0.2827 \text{ m}^2$
- Free space with sun

$$I_s \alpha A_s + P_{\text{int}} = \epsilon \sigma A_{\text{rad}} T^4 \Rightarrow T = \left(\frac{I_s \alpha A_s + P_{\text{int}}}{\epsilon \sigma A_{\text{rad}}} \right)^{1/4} = 362^\circ K$$



AERCam/SPRINT (LEO Cargo Bay)

- $T_{env} = 280^\circ K$
- LEO cargo bay, no sun

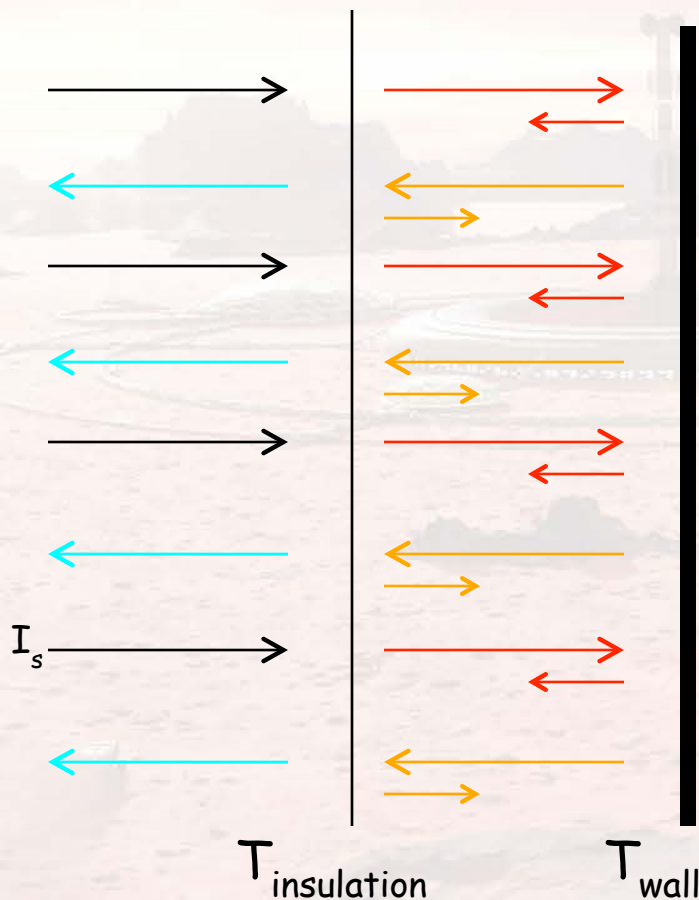
$$P_{int} = \epsilon \sigma A_{rad} (T^4 - T_{env}^4) \Rightarrow T = \left(\frac{200W}{0.8 \left(5.67 \times 10^{-8} \frac{W}{m^2 \cdot K^4} \right) (0.2827 m^2)} + (280^\circ K)^4 \right)^{1/4} = 384^\circ K$$

- LEO cargo bay with sun

$$I_s \alpha A_s + P_{int} = \epsilon \sigma A_{rad} (T^4 - T_{env}^4) \Rightarrow T = \left(\frac{I_s \alpha A_s + P_{int}}{\epsilon \sigma A_{rad}} + T_{env}^4 \right)^{1/4} = 391^\circ K$$



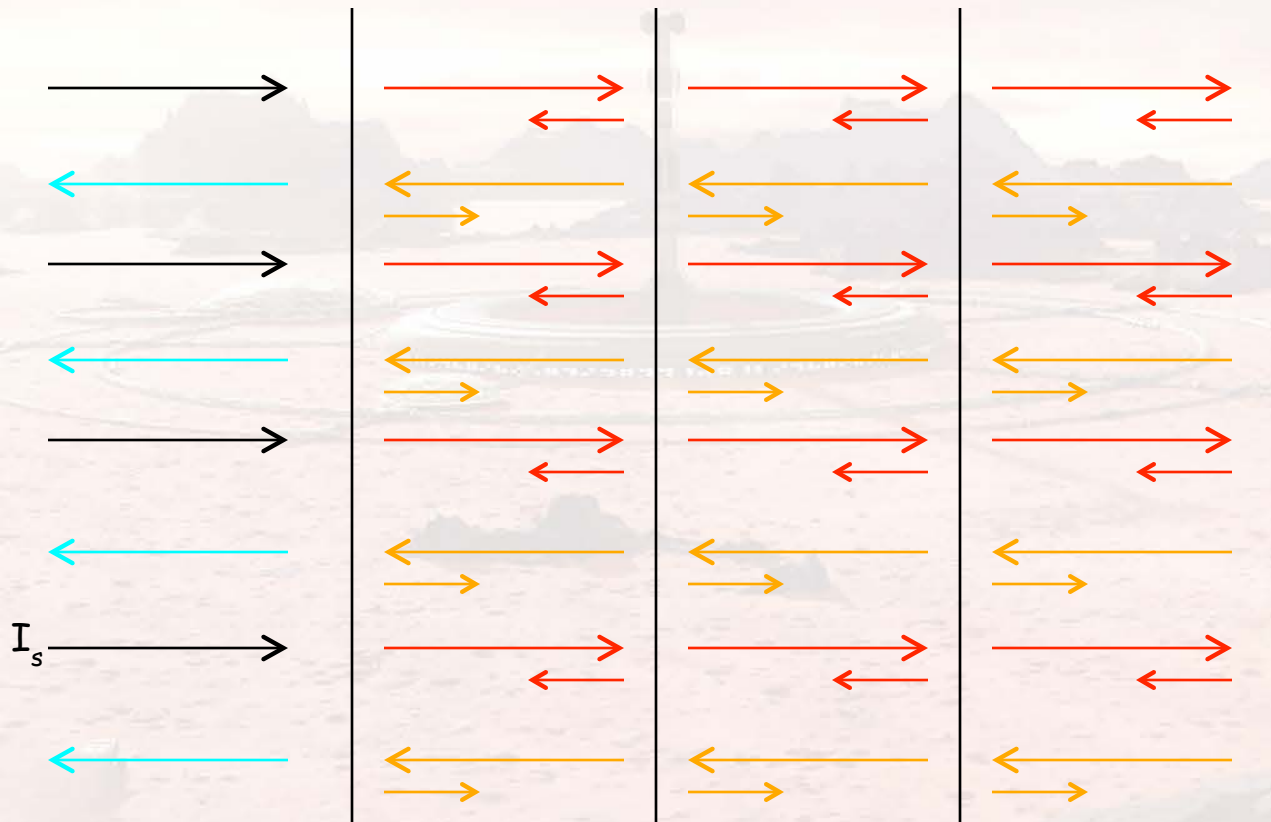
Radiative Insulation



- Thin sheet (mylar / kapton with surface coatings) used to isolate panel from solar flux
- Panel reaches equilibrium with radiation from sheet and from itself reflected from sheet
- Sheet reaches equilibrium with radiation from sun and panel, and from itself reflected off panel



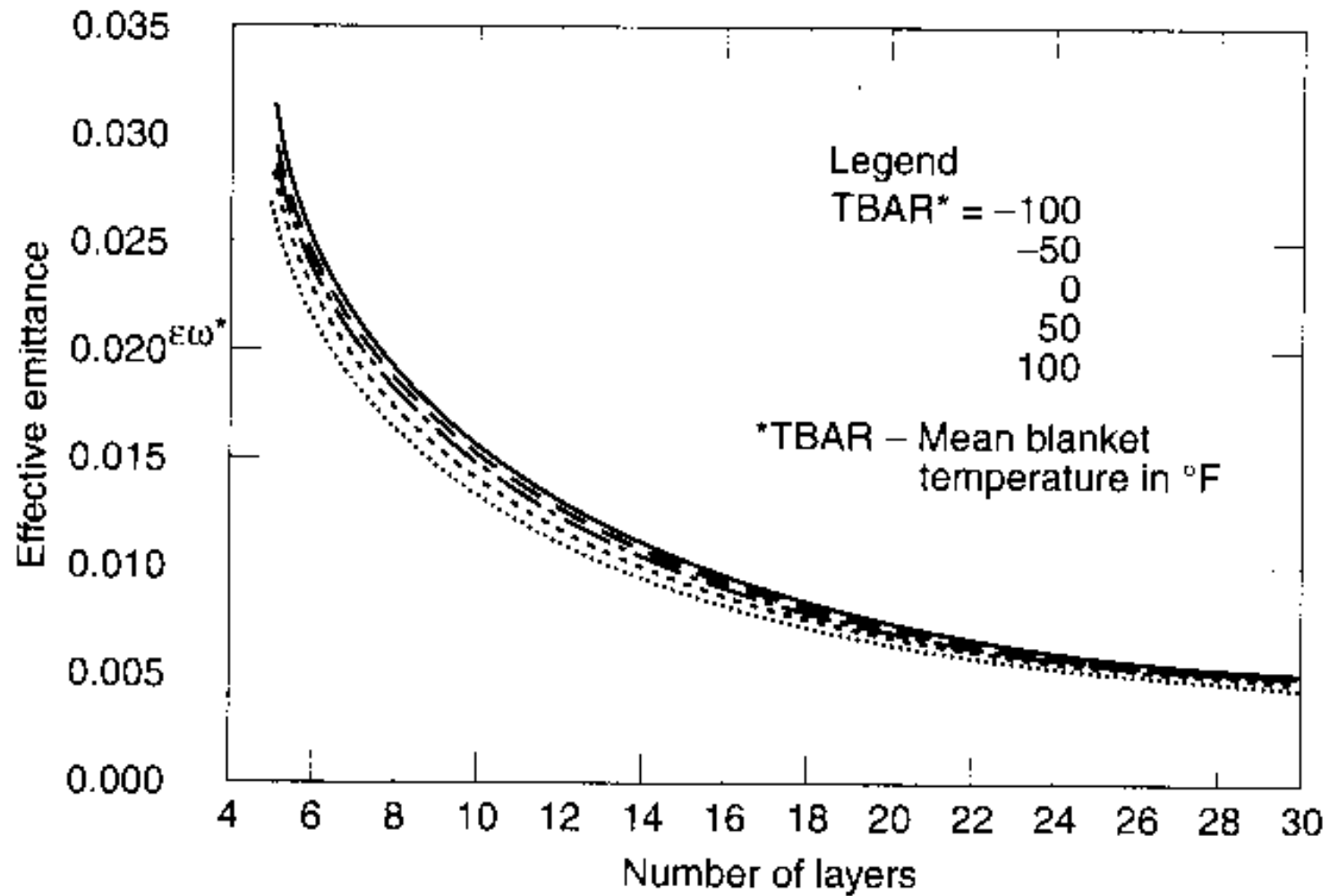
Multi-Layer Insulation (MLI)



- Multiple insulation layers to cut down on radiative transfer
- Gets computationally intensive quickly
- Highly effective means of insulation
- Biggest problem is existence of conductive leak paths (physical connections to insulated components)



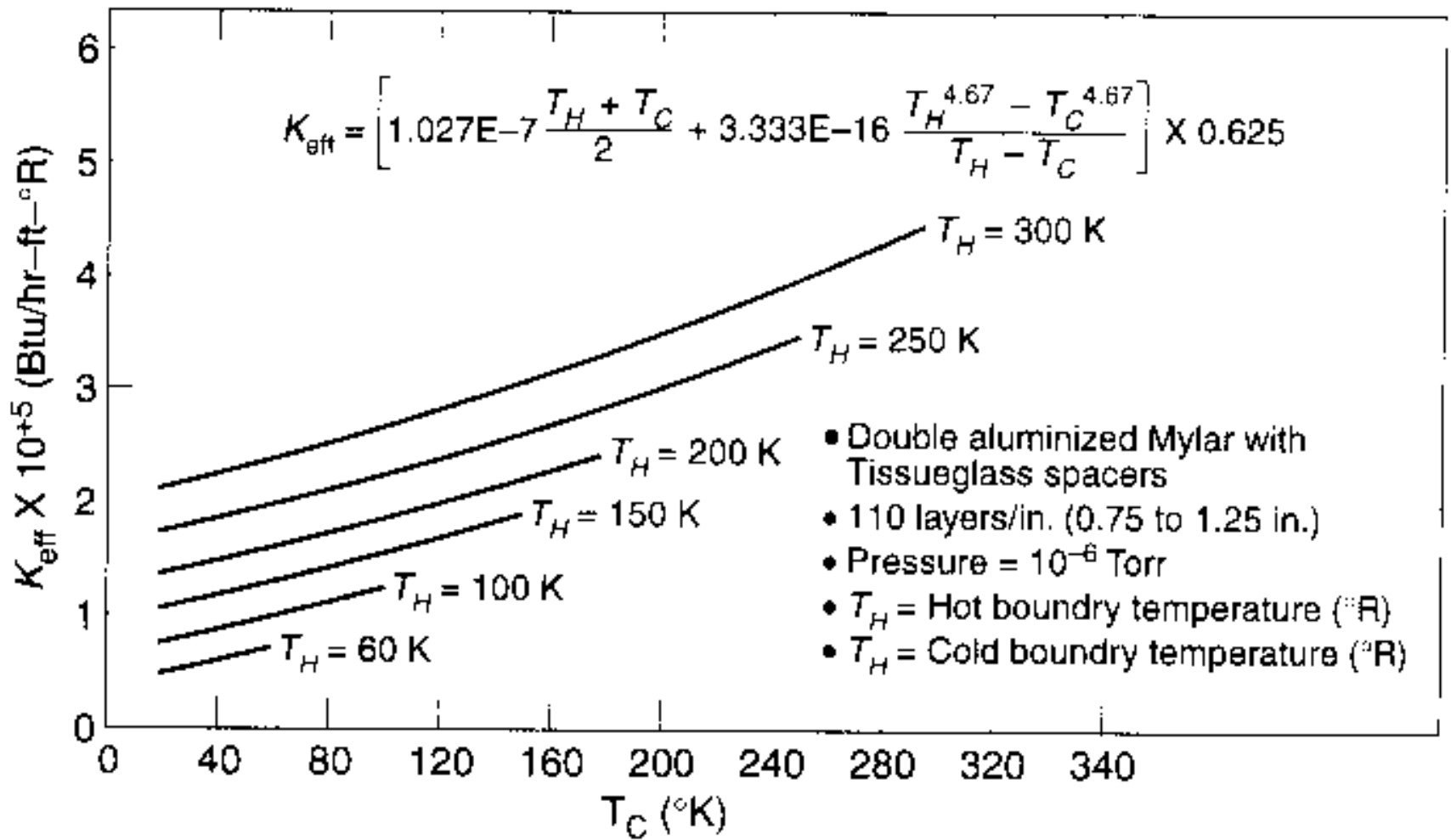
Emissivity Variation with MLI Layers



Ref: D. G. Gilmore, ed., Spacecraft Thermal Control Handbook AIAA, 2002



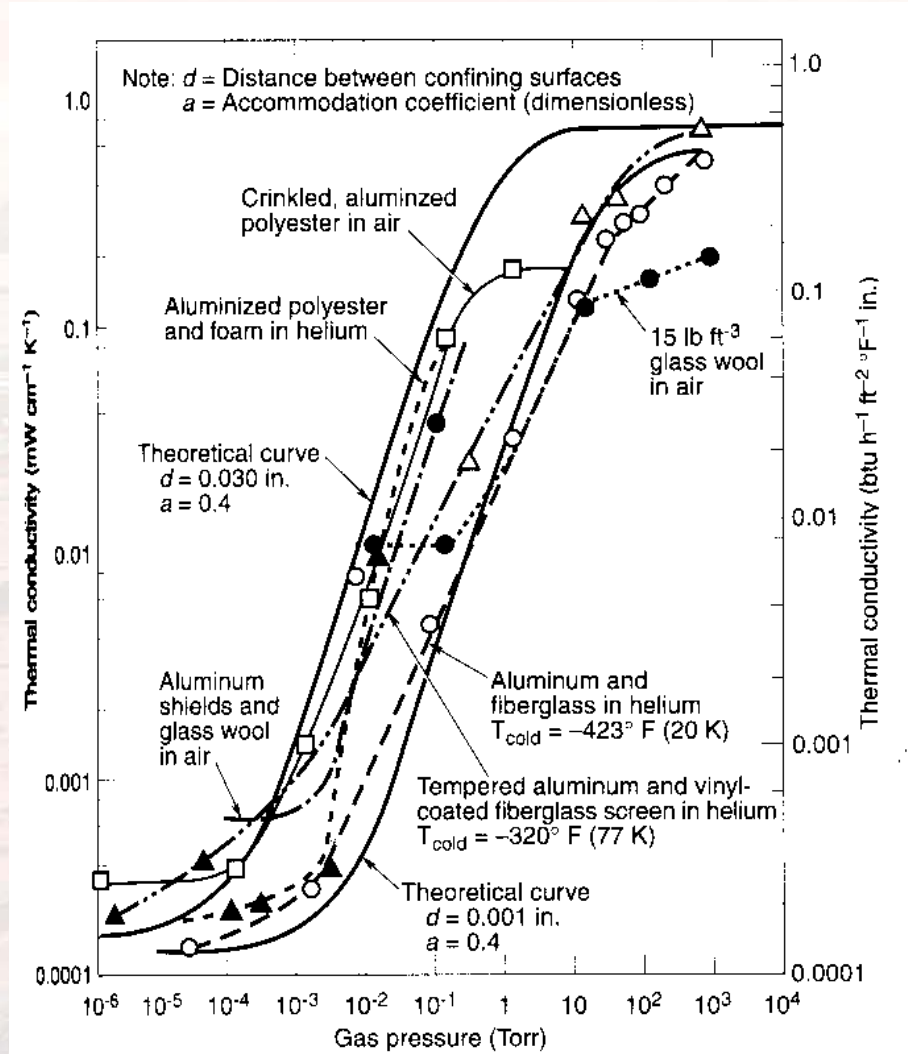
MLI Thermal Conductivity



Ref: D. G. Gilmore, ed., Spacecraft Thermal Control Handbook AIAA, 2002



Effect of Ambient Pressure on MLI



Ref: D. G. Gilmore, ed., Spacecraft Thermal Control Handbook AIAA, 2002



1D Conduction

- Basic law of one-dimensional heat conduction (Fourier 1822)

$$Q = -KA \frac{dT}{dx}$$

where

K=thermal conductivity (W / m°K)

A=area

dT / dx=thermal gradient



3D Conduction

General differential equation for heat flow in a solid

$$\nabla^2 T(\mathbf{r}, t) + \frac{g(\mathbf{r}, t)}{K} = \frac{\rho c}{K} \frac{\partial T(\mathbf{r}, t)}{\partial t}$$

where

$g(\mathbf{r}, t)$ = internally generated heat

ρ = density (kg/m³)

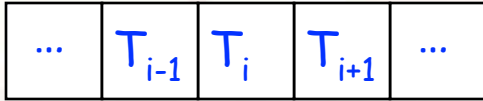
c = specific heat (J/kg[°]K)

$K/\rho c$ = thermal diffusivity



Simple Analytical Conduction Model

- Heat flowing from (i-1) into (i)



$$Q_{in} = -KA \frac{T_i - T_{i-1}}{\Delta x}$$

- Heat flowing from (i) into (i+1)

$$Q_{out} = -KA \frac{T_{i+1} - T_i}{\Delta x}$$

- Heat remaining in cell

$$Q_{out} - Q_{in} = \frac{\rho c}{K} \frac{T_i(j+1) - T_i(j)}{\Delta t}$$



Finite Difference Formulation

- Time-marching solution

$$T_i^{n+1} = T_i^n + d(T_{i+1}^n - 2T_i^n + T_{i-1}^n)$$

where

$$d = \frac{\alpha \Delta t}{\Delta x^2} \quad \alpha = \frac{k}{\rho C_v} = \text{thermal diffusivity}$$

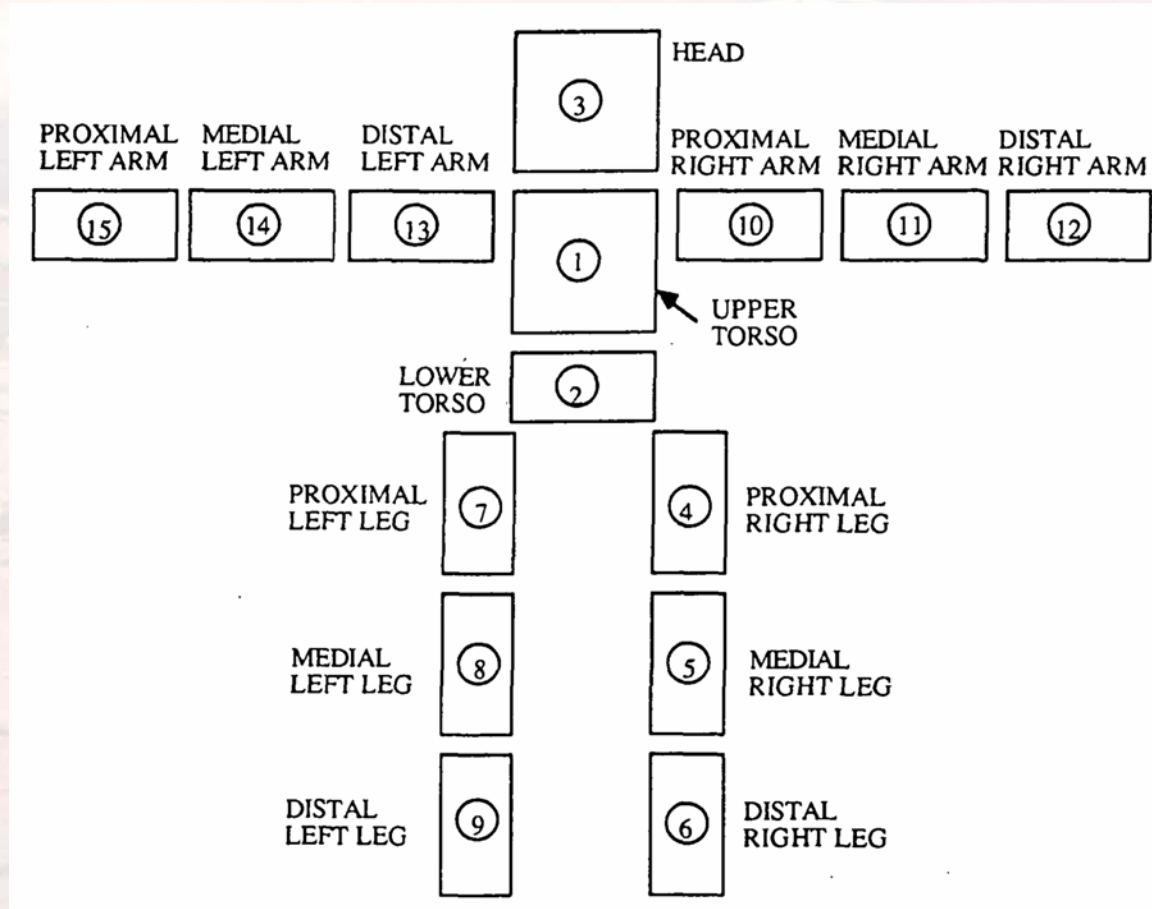
- For solution stability,

$$\Delta t < \frac{\Delta x^2}{2\alpha}$$



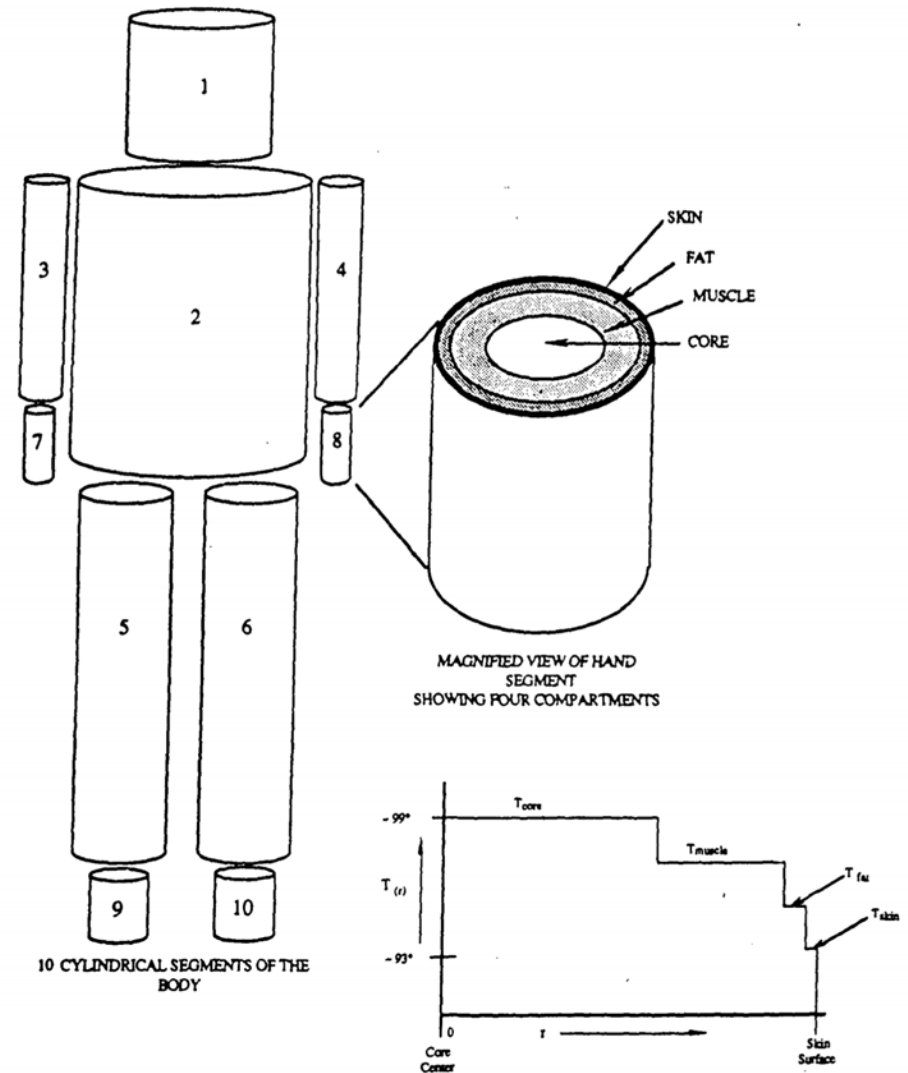
Human Thermal Model (Wissler)

- 15 elements per body
- 15 nodes per element
- Additional elements:
e.g., skin, sweat, air circulation
- ~300 nodes in full model



Human Thermal Model (METMAN)

- 10 element in body
- 4 nodes per element
 - Skin
 - Fat
 - Muscle
 - Core
- Blood is separate node
- 41 nodes total



Energy Balance in Each Node

$$Q_{st} = Q_m - Q_c - Q_r - Q_e - Q_k - Q_{resp} - Q_{LCG} = mc_P \frac{\partial T}{\partial t}$$

- Q_{st} - heat rate saved into tissue
- Q_m - heat rate due to internal metabolism
- Q_c - heat rate due to surface convection
- Q_r - heat rate due to radiative losses
- Q_e - heat rate due to evaporation
- Q_k - heat rate due to conduction to other nodes
- Q_{resp} - heat rate due to respiratory cooling
- Q_{LCG} - heat rate due to liquid cooling garment



41-Node Heat Flow Equations (1)

Core layer:

$$M_c C p_c \frac{dT_c}{dt} = \dot{m}_{b \rightarrow c} C p_b (T_b - T_c) + G_{m \leftrightarrow c} (T_m - T_c) + \dot{Q}_{\text{met}} - \dot{Q}_{\text{resp}}$$

Muscle layer:

$$M_m C p_m \frac{dT_m}{dt} = \dot{m}_{b \rightarrow m} C p_b (T_b - T_m) + G_{c \leftrightarrow m} (T_c - T_m) + G_{f \leftrightarrow m} (T_f - T_m) + \dot{Q}_{\text{met}} - \dot{Q}_{\text{shiv}} - \dot{Q}_{\text{resp}}$$

from Campbell, French, Nair, and Miles, "Thermal Analysis and Design of an Advanced Space Suit"

J. Thermophysics and Heat Transfer, v.14 n.2, April-June 2000



41-Node Heat Flow Equations (2)

Fat layer:

$$M_f C p_f \frac{dT_f}{dt} = \dot{m}_{b \rightarrow f} C p_b (T_b - T_f) + G_{m \leftrightarrow f} (T_m - T_f) \\ + G_{s \leftrightarrow f} (T_s - T_f) + \dot{Q}_{\text{met}} - \dot{Q}_{\text{resp}}$$

Skin layer:

$$M_s C p_s \frac{dT_s}{dt} = \dot{m}_{b \rightarrow s} C p_b (T_b - T_s) + G_{f \leftrightarrow s} (T_f - T_s) \\ + \dot{Q}_{\text{met}} - \dot{Q}_{\text{lat}} - \dot{Q}_{\text{LCG}} - \dot{Q}_{\text{VG}} - \dot{Q}_{\text{suit}}$$

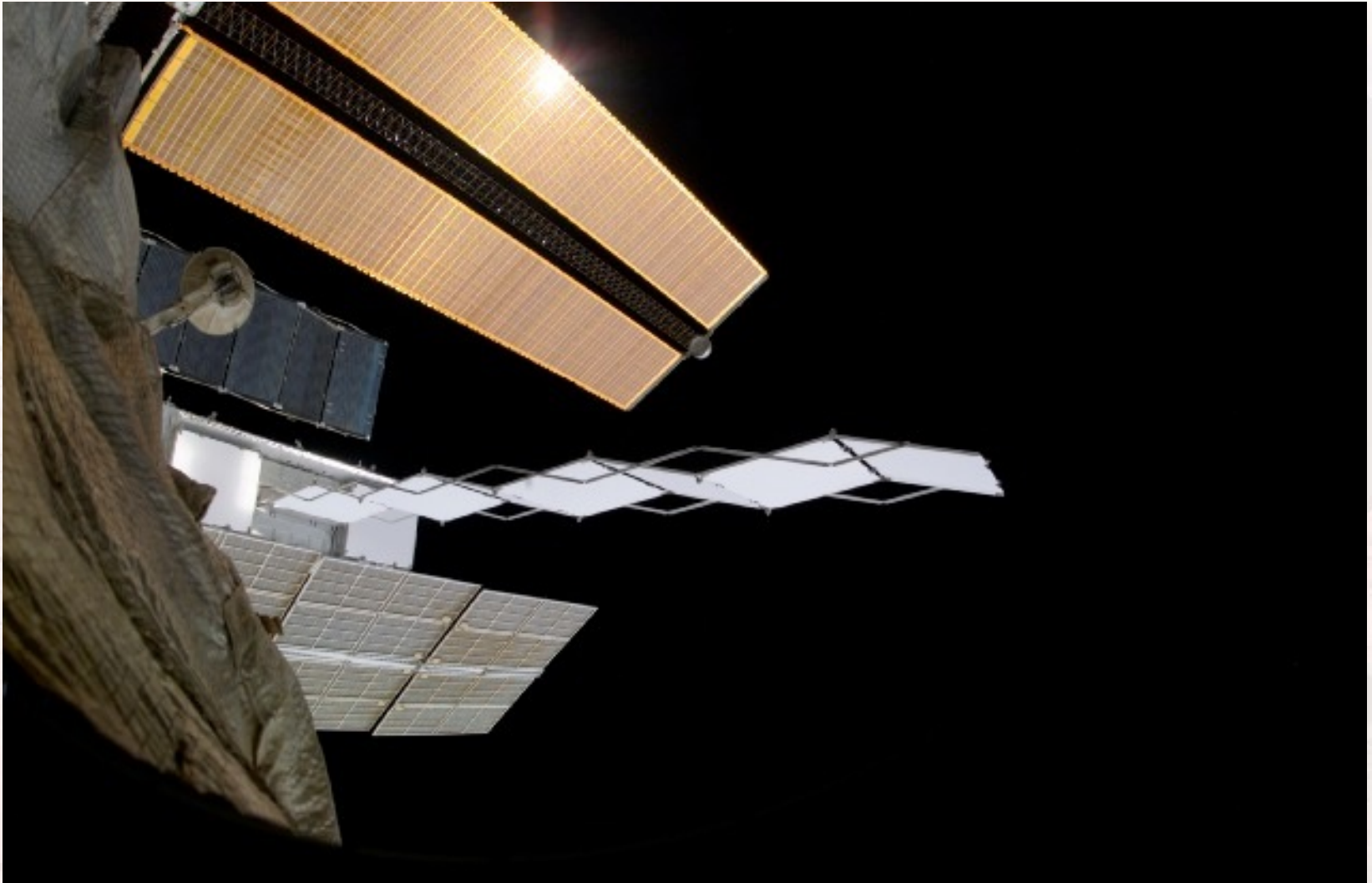
Blood pool:

$$M_b C p_b \frac{dT_b}{dt} = C p_b \sum_{i=1}^{10} \sum_{j=1}^4 \dot{m}_{b \rightarrow i,j} (T_{i,j} - T_b)$$

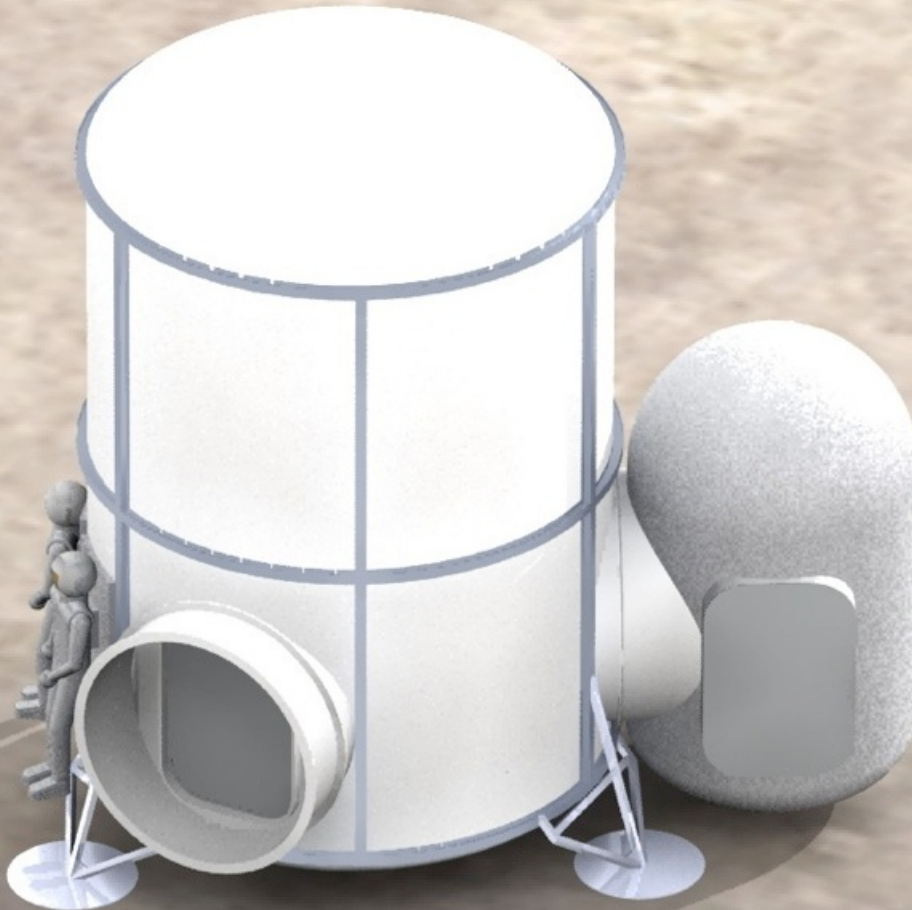
from Campbell, French, Nair, and Miles, "Thermal Analysis and Design of an Advanced Space Suit"
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ISS Radiator Assembly



Case Study: ECLIPSE Thermal Analysis



- Developed by UMd SSL for NASA ESMD
- Minimum functional habitat element for lunar outpost
- Radiator area - upper dome and six upper cylindrical panels



ECLIPSE Heat Sources

- Solar heat load (modeling habitat as right circular cylinder)

$$A_{illuminated} = \ell d \sin \beta + \frac{1}{4} \pi d^2 \cos \beta$$

$$Q_{solar} = A_{illuminated} \alpha I_s$$

- Electrical power load = 4191 W
- Metabolic work load (4 crew) = 464 W



Thermal Modeling for Lunar Surface

- Assume upper dome radiates only to deep space
- Assume side panels radiate half to deep space and half to lunar surface
- Assume (conservatively) that lunar surface radiates as a black body

$$Q_{internal} + Q_{solar} = \epsilon\sigma \left[A_{dome}T_{rad}^4 + n_{rad}A_{panel} \left(T_{rad}^4 - \frac{1}{2}T_{moon}^4 \right) \right]$$

$$T_{rad} = \left[\frac{1}{A_{dome} + n_{rad}A_{panel}} \left(\frac{Q_{internal} + Q_{solar}}{\epsilon\sigma} + \frac{1}{2}n_{rad}A_{wall}T_{moon}^4 \right) \right]^{\frac{1}{4}}$$



ECLIPSE Thermal Results

Case	Solar Angle (deg)	Lunar Surface Temp (K)	Active Panels	Wall	Radiator Temp (K)
Polar Outpost Day	88	180	3		283
Local Midnight	N/A	120	1		285
Typical Mid-latitude	45	215	4		287
Equatorial Noon	0	380	6†		290

†Radiator geometry modified to reduce total lunar surface exposure

